

Introduction to Fluid Mechanics:

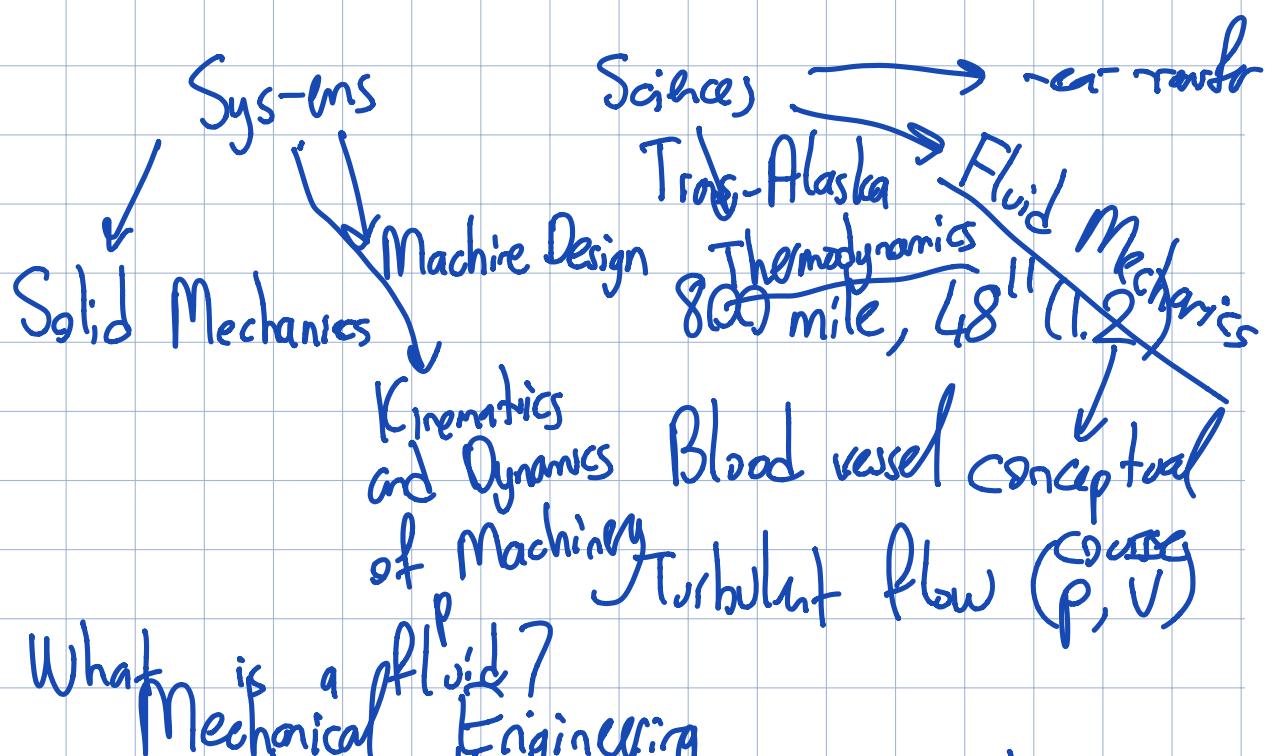
Aerospace

Civil

mechanical

electrical / computer

chemical



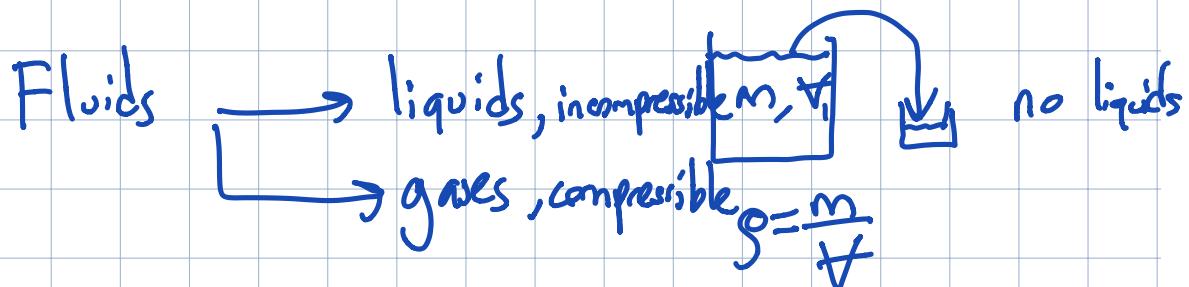
a substance that deforms continuously when sheared \downarrow tangential forces

Water, Oil, air, honey, toothpaste, paint

Solid \leftrightarrow fluids

shear stress \rightarrow small deformation in solids
 \rightarrow fluids infinite deformations

intermolecular forces \rightarrow strong in solids
weaker in fluids



Systems of Units

\rightarrow (SI)

force \rightarrow Newton (N)

length \rightarrow meter (m)

time \rightarrow seconds

mass \rightarrow kg

$\text{L} \rightarrow (\text{BG})$ δ
 force \rightarrow pounds (lb)
 length \rightarrow foot (ft)
 time \rightarrow seconds
 mass \rightarrow slug

Important Fluid Properties and Definitions:

Density (ρ) $\rho = \frac{m}{v}$ velocity
volume

liquids mass \rightarrow volume density is constant for liquids

gases mass \rightarrow { constant
Volume density is variable
for gases

Specific Weight: (γ)

$$\gamma = g \cdot \rho$$

accel. due to gravity

Specific Gravity (S.G.)

$$S.G. = \frac{\rho}{\rho_{\text{water at } 4^\circ\text{C}}}$$

$$\begin{aligned} S.G. &= 13,600, \\ &= 13.6 \end{aligned}$$

Pressure (P)

$$\cancel{\frac{\text{Force}}{\text{area}}}$$

$$\frac{F}{A} = P$$

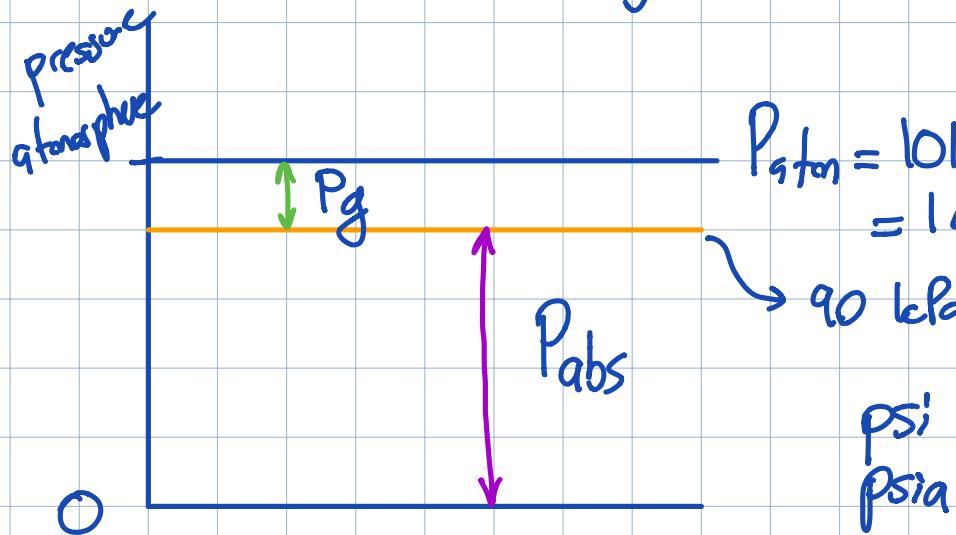
$$P = \frac{F \cdot \cos \alpha}{A}$$

$$\frac{\text{Normal force component}}{\text{area}} = P$$

2 ways of representing pressure

1) Absolute pressure (P_{abs}) datum zero pressure
vacuum

2) Gage pressure (P_g) datum atmospheric pressure



$$P_{abs} = 90 \text{ kPa}$$

$$P_g = P_{abs} - P_{atm}$$

$$= (90 - 101.325)$$

$$= -11.325 \text{ kPa}$$

$$(P_{atm})_{abs} = 101.325 \text{ kPa}$$

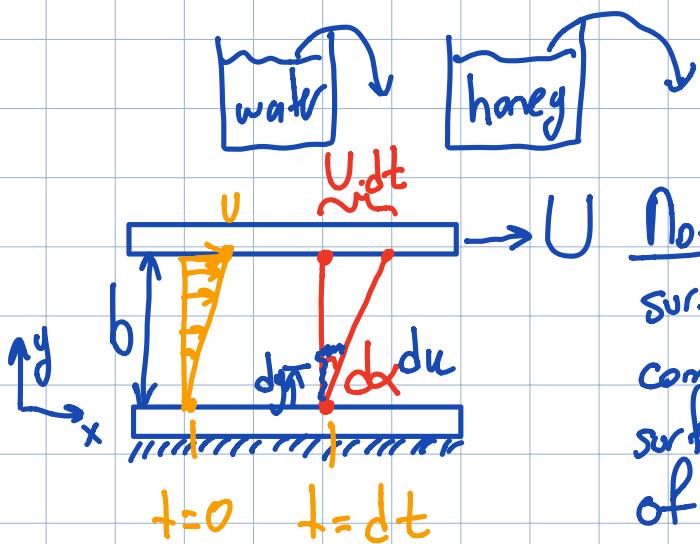
$$(P_{atm})_g = 0 \text{ Pa}$$

Viscosity: Fluidity

5W30

0W40

Quantifies the resistance of a fluid being sheared!



No-slip condition: At a solid surface, the fluid velocity component tangent to the surface is equal to that of the surface

$$\tau_{\text{fluid}} = \frac{U dt}{b} = \frac{du \cdot dt}{dy}$$

$$b dx = dx$$

$$dx = \frac{du \cdot dt}{du}$$

$$\frac{dx}{dt} = \frac{du}{du} = \frac{U}{L}$$

Newton's law of viscosity: the shear stress on a surface tangent to the flow direction is proportional to the rate of change shear strain ($\frac{dx}{dt}$)

$$\left[\begin{array}{c} w \\ y \end{array} \right] \propto$$

$$\frac{dx}{dt} = \frac{du}{dy}$$

$$\boxed{\gamma_w = \nu \cdot \frac{du}{dy}}$$

for newtonian liquids

$\nu \rightarrow$ absolute viscosity, dynamic viscosity

$$\frac{\partial \nu}{\partial T} \rightarrow \begin{cases} \text{liquid} & \frac{\partial \nu}{\partial T} < 0 \\ \text{gases} & \frac{\partial \nu}{\partial T} > 0 \end{cases}$$

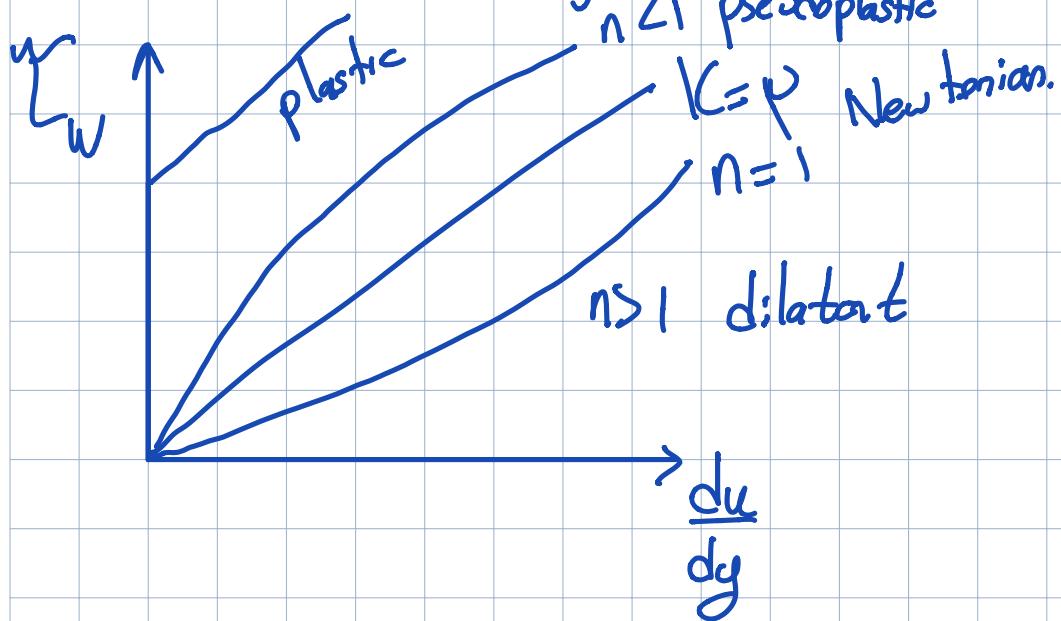
$$\eta = \frac{\nu}{\rho} \quad \text{kinematic viscosity}$$

Inviscid flow $\Rightarrow (\rho=0)$

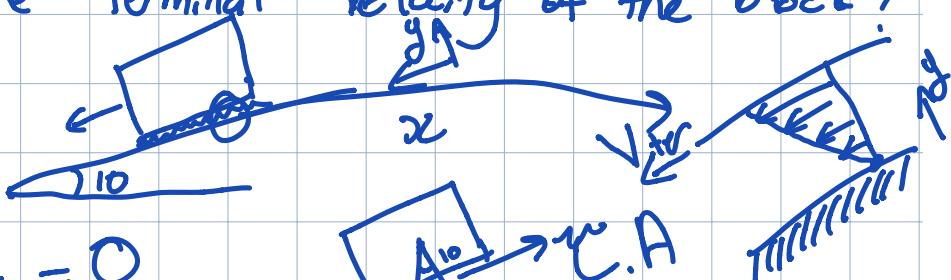
Ostwald-de Waele power-law

$$\dot{\gamma}_w = K \left(\frac{du}{dy} \right)^n$$

$K=p \quad n=1$



Example: A 1 kg block slides down 10° inclined surface with 1 mm thick glycerin between the block and the inclined surface. If the block makes a 1m^2 contact with the oil, find the terminal velocity of the block?



$$\sum F_x = 0$$

$$W \cdot \sin 10 - v \cdot A = 0$$

$$\downarrow p \cdot \frac{du}{dy}$$

$$W \cdot \sin 10 - p \cdot \left(\frac{du}{dy} \right) \cdot A = 0$$

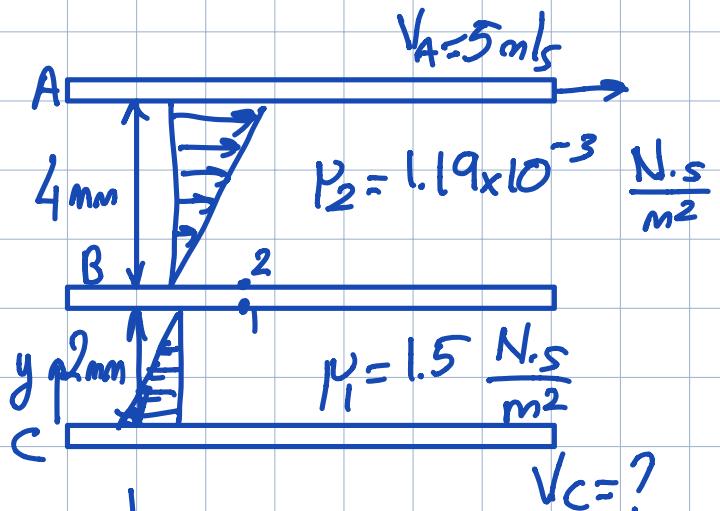
$$\frac{du}{dy} = \frac{U}{b}$$

$$mg \sin 10 - (1.5) \frac{V_{terr}}{(10^{-3})} \cdot (1) = 0$$

$$1 (9.81)$$

$$V_{terr} = 0.0011 \text{ m/s}$$

There are three parallel plates in the system as illustrated in the figure below. The top plate A moves to the right with a constant velocity of 5 m/s, while the plates B is stationary. All the necessary fluid properties and parameters are illustrated in the figure. What should be the speed and direction of plate C?



$$\textcircled{1} \quad \mu_1 = P_1 \cdot \frac{dU_1}{dy}$$

$$\textcircled{1} \quad \mu_1 \cdot \cancel{P_1} = F \leftarrow$$

$$\textcircled{2} \quad \mu_2 = P_2 \cdot \frac{dU_2}{dy}$$

$$\textcircled{2} \quad \mu_2 \cdot \cancel{P_2} = F \leftarrow$$

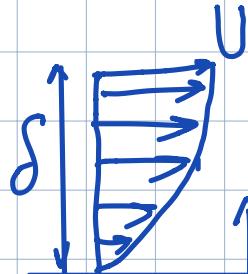
$$\left(\mu_1 \cdot \frac{dU_1}{dy} \right) = \left(\mu_2 \cdot \frac{dU_2}{dy} \right)$$

$$\therefore \textcircled{1} \quad \textcircled{2} \quad \frac{5}{1} \quad \frac{2}{2}$$

$$(1.5) \left(\frac{U - V}{2 \times 10^{-3}} \right) = (1.19 \times 10^{-3}) \left(\frac{5 - V}{4 \times 10^{-3}} \right)$$

$$-3V = (5)(1.19 \times 10^{-3}) \Rightarrow V = -0.02 \text{ m/s}$$

Wind passing the top of a building creates a boundary layer. The velocity profile within the boundary layer is as shown in the figure below. Determine the magnitude of the force exerted on the building as a function of the boundary layer thickness (δ), wind velocity (U) and the surface area of the building (A). Take the viscosity of air as $18 \times 10^{-6} \frac{\text{N.s}}{\text{m}^2}$.



$$\frac{u(y)}{U} = 2 \left(\frac{y}{\delta} \right) - \left(\frac{y}{\delta} \right)^2$$

$$F = p \cdot \frac{du}{dy} \quad u(y) = \left[2 \left(\frac{y}{\delta} \right) - \left(\frac{y}{\delta} \right)^2 \right] U$$

$$\frac{du}{dy} = U \cdot \left[\frac{2}{\delta} - \frac{2y}{\delta^2} \right]$$

y

$[0 \quad \delta]$

$$\tau = p \cdot U \left[\frac{2}{\delta} - \frac{2y}{\delta^2} \right]$$

$$\tau \cdot A = F = p \cdot U \cdot A \left[\frac{2}{\delta} - \frac{2}{\delta^2} \cdot y \right]$$

$$F \Big|_{y=0} = p \cdot U \cdot A \left[\frac{2}{\delta} - \frac{2}{\delta^2} \cancel{\Big|_y} \right] \Big|_{y=0}$$

$$F = \frac{2 \cdot p \cdot U \cdot A}{\delta}$$

$$F = \frac{(36 \times 10^{-6}) U \cdot A}{\delta}$$

Compressibility of Fluids :

Measure of how the volume (∇) of a given mass of a fluid changes w.r.t Pressure.

Characterized by bulk modulus, $E_V = -\frac{dp}{d\nabla}$

Gases are highly compressible.

Liquids are incompressible

Compression / Expansion \rightarrow constant T
isothermal process

$$\frac{P}{g} = \text{const}$$

Compression / Expansion \rightarrow frictionless, no heat exchange
with the surrounding
isentropic process

$$\frac{P}{g^k} = \text{const}$$

$$k = \frac{C_p}{C_v}$$

k: specific heat ratio

~ .0 1 1 1 1 1 D

C_p : specific heat at constant T

C_v : specific heat at constant Volume

$$R = C_p - C_v$$

Mach Number $M = \frac{V}{C}$

$$C = \sqrt{\frac{C_v}{g}}$$

$$C = \sqrt{kRT}$$
 isentropic process

$$C = 343 \text{ m/s air}$$

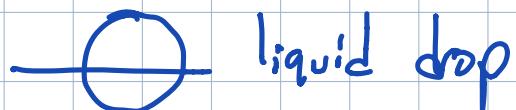
$$C = 1481 \text{ m/s water}$$

$M < 0.3$ compressibility effects are negligible.

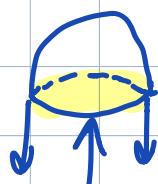
Surface Tension: σ

measure of the force at the interface between

2 immiscible fluids



liquid drop



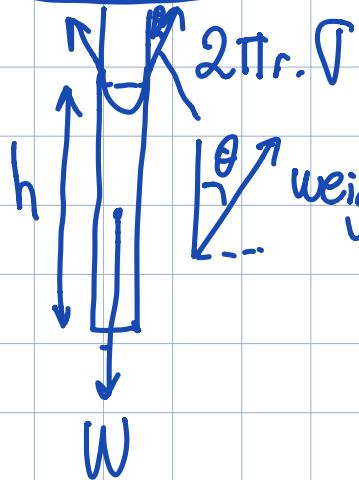
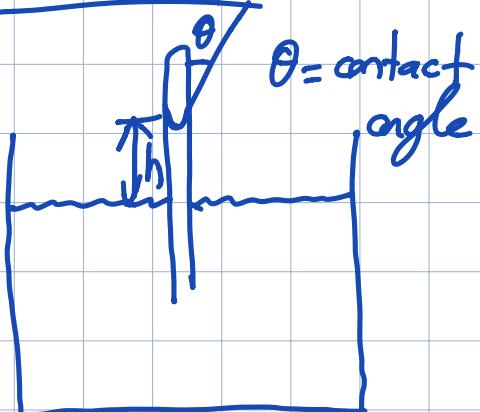
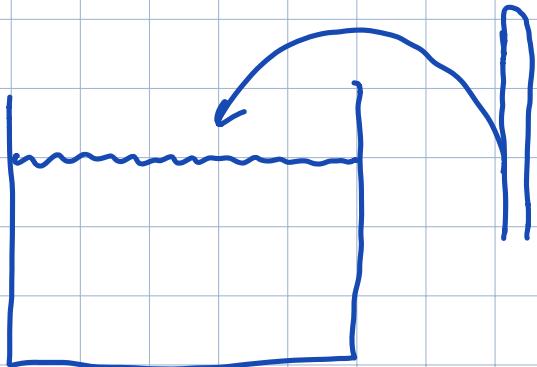
$$\sigma \cdot (2\pi r)$$

$$\Delta p \cdot \pi r^2$$

$$\sigma \cdot 2\pi r = \Delta p \cdot \pi r^2$$

$$\Delta p = \frac{2V}{r}$$

$$\Delta p = \frac{4V}{D}$$



$$g = \frac{M}{A}$$

$$\text{weight} = mg = g \cdot A \cdot g = \gamma \cdot A \cdot (πr^2) \cdot h$$

$$2\pi r \cdot \gamma \cdot \cos \theta = \gamma \cdot \pi r^2 \cdot h$$

$$h = \frac{2 \cdot \gamma \cdot \cos \theta}{\gamma \cdot r}$$